

# SHORT TERM SCIENTIFIC MISSION (STSM) - SCIENTIFIC REPORT

The STSM applicant submits this report for approval to the STSM coordinator

Action number: CM1404 **STSM title: SMARTCATS** 

STSM start and end date: 29/10/2018 to 02/11/2018

Grantee name: Dr. Kieran P. Somers

# PURPOSE OF THE STSM

This STSM is a follow-up to a previous STSM attended by Dr. Ultan Burke and Dr. Matteo Pelucchi, also hosted in RWTH Aachen by Prof. Pitsch. This is the first STSM for this particular researcher (Dr. Kieran Somers)

Following the successful STSM in Aachen in July, focusing on the collation, critical evaluation and design of a working process for efficient review, the current STSM expands upon the number of reactions under consideration and on the methods themselves, in order to garner relevant insight into the statistical evaluation of large sets of data. Ultimately, the goal of this collaboration between COST partners and external partners (National University of Ireland Galway (NUIG), Politecnico di Milano (PoliMi), RWTH Aachen, Argonne National Laboratory (ANL), Denmark Technical University (DTU) and ELTE Budapest) to collect, collate, evaluate and reconcile conflicting results for the existing data within the literature for hydrogen/syngas oxidation, is producing an outcome of outstanding relevance for the entire kinetic modelling community, by compiling the results of the review, into recommendations for each of the elementary reactions. The final outcome will be a kinetic model which is an accurate reflection of our most up to date understanding of the chemical kinetics for such system. This will also ensure that the obtained model can predict the indirect data of interest for more practical application such as, ignition delay times and laminar burning velocities.

The detail of the objectives of this STSM are listed below:

- 1) Consistently format the data collected over the previous 21 months to facilitate dissemination and interpretation. Statistics on the number of data/paper collected are provided in this report.
- 2) Discuss the most suitable methods to perform mathematical fitting of rate constants based on theoretical and experimental determinations. Details of the approach for pressure-dependent reactions are given in this report, and details of the approach used for pressure-independent reactions are provided in the reports of Dr. Ultan Burke, and Dr. Matteo Pelucchi.
- 3) Discuss and provide meaningful methods to define uncertainties.
- 4) Provide an outline for the treatment of every elementary reaction that is suitable for publication and easy use by kinetic modelers and users of kinetic models
- 5) Discuss and provide appropriate treatments of pressure dependent reactions
- 6) Provide a recommendation for additional reactions within the hydrogen/syngas model (OH+OH<=>O+H<sub>2</sub>O was specific to this researcher, as well as the collection and organization of the

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large amount of information on  $HO_2+HO_2=H_2O_2+O_2$  and HCO+M that was useful to guide a proper treatment of pressure dependent reactions)

Together with these objectives, useful discussions allowed to further improve and extend the methods and approaches defined in the previous meeting. As part of this STSM, this author has contributed to the management of the project, to the collation of data for key reactions, and to the development of a method to fit pressure-dependent rate measurements based on theoretical modelling results.

### DESCRIPTION OF WORK CARRIED OUT DURING THE STSMS

#### Project Management and Project Overview

Project management is a critical component of any project in order to meet targets, and assess progress on an ongoing basis. As the current project is unfunded (with the exception of COST support), involves collocated teams of people with varying expertise, some aspects of project management are necessary to delegate workload amongst contributors, and to assess on-going progress. As part of the current STSM, the current author spent ~20% of their time (1 out of 5 days) familiarising with the procedures and workflows established by the working group as part of their previous COST STMS which was held in Aachen in July 2018. All of the papers and data which were collated as part of the previous STSM were organised into a structured database by this author. Project Gannt Charts and workflows were then constructed to allow the team members to co-ordinate and collaborate effectively and to allow for the project to be managed on a longer term basis when collaborators returned to their home institution. A set of computational tools which manage and analyse the database of papers, and corresponding experimental data were also constructed during this time. The results section of this report provides an overview of the project, the results of which are directly relevant to COST SMARTCATS WG1 – "Smart energy carriers gas phase chemistry: from experiments to kinetic models", and also WG4 – "Standard definition for data collection and mining toward a virtual chemistry of smart carriers".

## Data Collection and Tabulation for H2 ⇔H+H

Approximately 20% (1/5 days) of the current authors STSM was designated to collating data for reaction R2 (H+H+M⇔H2+M). This recombination reaction is an important initiation and termination reaction in combustion systems, and is also the simplest combustion reaction possible. In total, there are 36 experimental rate constant recommendations, 4 theoretical rate constant recommendations, and 1 rate constant recommendation based on detailed chemical kinetic modelling studies, Figure 1. The data must be digitized in order to arrive at a rate constant recommendation, and this will take place as part of future work.

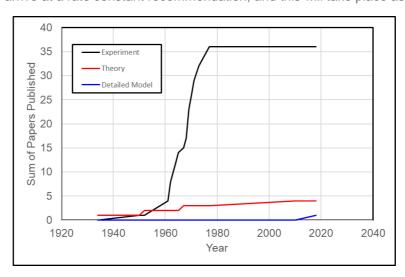


Figure 1: Cumulative number of papers published on the reaction H+H+M<=>H<sub>2</sub>+M



#### Data Fitting for Pressure-Dependent Reactions

Of the 50 reactions being considered as part of *this work*, 33 reactions (66%) involve bimolecular reactions proceeding through a single transition state forming bimolecular products, and 17 reactions (33%) involve an energised adduct, which can undergo non-reactive bimolecular collision which transfers ro-vibrational energy between the adduct and collider. Whilst the former 33 reactions tend to be only temperature dependent, those 17 reactions which involve collisional energy transfer (CET) are both temperature- and pressure-dependent, and some form of complex model (e.g. Lindemann Model, Troe Model/Fit, RRKM/Master Equation) is required to interpolate and extrapolate data so that rate constants can be cast in a form that is useful for chemical kinetic modelling studies, but also, a form which is based on a physically meaningful model.

An approach to fitting the majority (66%) of reactions which are only temperature-dependent was developed during this STSM, the details of which are outlined in the report of Dr. Burke who validated a method based available data for the  $H+O_2=O+OH$  system, which is the most important reaction in combustion. In the case of reactions which are both temperature- and pressure-dependent, data tends to be sparse over all regimes of temperature/pressure/diluent space which is relevant for combustion. A suitable method to fit experimental data is a much more complex task than for reactions which are only temperature-dependent, as the fitting method must retain a fundamentally physical basis such that extrapolation beyond experimental measurement is accurate.

Therefore ~60% (3/5 days) of the current STSM was designated to discuss and design a suitable data-fitting approach for the 17 reactions which are both temperature and pressure-dependent, which ultimately requires a tabulation of all available experimental data and conditions (temperature, pressure, rate constant, collider) coupled with ab initio quantum chemistry/statistical rate theories (RRKM/ME). Dr. Somers and Dr. Pelucchi, in collaboration with Dr. Klippenstein, have tabulated experimental data for two key combustion reactions which have been well-studied experimentally: H+CO+M=HCO and HO<sub>2</sub>+HO<sub>2</sub>=H<sub>2</sub>O<sub>2</sub>+O<sub>2</sub>. A detailed potential energy surface (PES) must first be constructed based on accurate ab initio methods. An important contribution of Dr. Klippenstein to this project is the provision of the PES for each reaction classified in the following section of this report. Once the PES has been characterised the experimental data must be provided to a RRKM/ME solver in order for some form of error-minimised fitting to be carried out. As part of this STSM, the current author built a computational tool in order to automatically carry out large-scale RRKM/ME calculations in order to fit available data. The approach is still under development as the errorminimisation approaches are more complex than a simple least-squares regression as the reaction barrier, the bath gas/collider properties, the energy transfer parameters, are all optimisable parameters. Preliminary results are presented in subsequent sections for conditions where the energy transfer parameters were used to fit the experimental data.



#### DESCRIPTION OF THE MAIN RESULTS OBTAINED

#### Project Management and Project Overview

Tables 2 and 3 below provide high-level synopses of the current status of the project with Table 1 providing a legend to interpret Gannt Charts and Task Completion Rates shown in Tables 2 and 3. Table 3 gives a reaction-specific breakdown of the current status. Each reaction is classified based on the number of electrons in the system, which is appropriate when considering reactions that take place on a multi-channel or multiple-well potential energy surface, where absolute rate constants may be sensitive to both pressure and temperature, and where relative rate constants (branching ratios) may also be of interest to kinetic modellers. For each reaction, lead investigator(s) are assigned, and a series of tasks must be completed before a reaction data-sheet is written (RDS) and the data sheet is peer-reviewed (DSPR) by all collaborators before final recommendations are made. These tasks are non-trivial and labour-intensive (sourcing and mining data), and includes exhaustive literature review to collate papers (PC), tabulation of experimental data (EDT), tabulation of theoretical data (TDT) before the rate constant can be fitted (RCF) and a rate constant with appropriate uncertainties recommended for use in combustion modelling.

Table 2 below show that approximately 37.5% of all tasks have been carried out when one analyses the set of 50 reactions of interest. The key tasks of PC, EDT, TBT, PES construction are ~50% complete.

Table 1: Legend for Table 2 and Table 3								
	Key/Legend	Authors Abbreviations						
PC	Papers Collated into Database	MP Dr. Matteo Pelucchi						
EDT	Experiment Data Tabulated	UB	Dr. Ultan Burke					
TDT	Theoretical Data Tabulated	LC	Dr. Liming Cai					
PES	Potential Energy Surface Constructed	SJK	Dr. Stephen J. Klippenstein					
SRT	Statistical Rate Theory Computed	PG	Prof. Peter Glarborg					
RCF	Rate Constant Fitted	KPS	Dr. Kieran P. Somers					
RDS	Reaction Data Sheet Written							
DSPR	DSPR Reaction Data Sheet Peer-Reviewed							
С	Completed							
IP	In Progress							
Х	To be Completed							

Table 2: Task Completion Summary Statistics										
Status	PC	ET	TT	PES	RRKM/ME	RCF	RDS	PR	Total %	
Completed	52%	48%	42%	54%	0%	4%	14%	0%	26.75%	
In Progress	0%	0	0%	0%	36%	34%	0%	16%	10.75%	
To be Completed	48%	52%	58%	46%	64%	62%	86%	84%	62.5%	
Completed/In Progress	52%	48%	42%	54%	36%	38%	14%	16%	37.5	



Table 3: Reaction Gannt Chart										
# Electrons	Reaction	Lead	РС	EDT	TDT	PES	RRKM/ME	RCF	RDS	DSPF
R2	H+H+M<=>H2+M	KPS/MP	С	Х	Х	С	Х	Х	Х	Х
R9	H+O+M<=>OH+M	KPS/MP	Х	Х	Х	С	Х	Х	Х	Х
R10a	H+OH+M<=>H2O	UB	Х	Х	Х	С	Х	Х	Х	Х
R10b	H2+O<=>OH+H	LC	С	С	Х	С	Х	IP	Х	Х
R11	H2+OH<=>H+H2O	MP	С	С	С	Х	IP	ΙP	Х	Х
R15	HCO+M<=>H+CO+M	KPS/SJK	С	С	С	Х	IP	IP	Х	Х
R16a	HCO+H<=>CH2O	KPS	Х	Х	Х	Х	Х	Х	Х	Х
R16b	HCO+H<=>CO+H2	MP	Х	Х	Х	Х	Х	Х	Х	Х
R16p	O+O+M<=>O2+M	KPS/MP	Х	Х	Х	Х	Х	Х	Х	Х
R17a	H+O2+M<=>HO2+M	SJK	С	С	С	Х	IP	Х	Х	Х
R17b	H+O2<=>O+OH	UB	С	С	С	Х	Х	С	Х	Х
R18a	OH+OH+M<=>H2O2+M	UB	С	С	С	С	Х	IP	Х	Х
R18b	OH+OH<=>O+H2O	LC	С	С	С	С	Х	С	Х	IP
R18c	H+HO2<=>H2+O2	PG	С	С	С	С	IP	Х	Х	Х
R18d	H+HO2<=>OH+OH	PG	С	С	С	С	IP	Х	Х	Х
R18e	H+H+O2<=>H2+O2	KPS/MP	Χ	Х	Х	С	IP	Х	Х	Х
R18f	H+H+O2<=>OH+OH	KPS/MP	Х	Х	Х	С	Х	Х	Х	Х
R19a	H2O2+H<=>H2O+OH	SJK	С	С	С	С	IP	IP	Х	Х
R19b	H2O2+H<=>HO2+H2	SJK	С	С	С	С	IP	IP	Х	Х
R22	CO+O+M<=>CO2+M	PG	Х	Х	Х	Х	Х	Х	Х	Х
R23a	H+CO2+M<=>HOCO+M	PG/SJK	С	С	С	С	Х	IP	Х	Х
R23b	CO+OH+M<=>HOCO+M	PG/SJK	С	С	С	С	Х	IP	Х	Х
R23c	CO+OH<=>CO2+H	PG/SJK	С	С	С	С	Х	Х	Х	Х
R23d	HCO+O<=>CO2+H	UB	Χ	Х	Х	С	Х	Х	Х	Х
R23e	HCO+O<=>CO+OH	UB	Х	Х	Х	С	Х	Х	Х	Х
R24a	HCO+OH<=>CO2+H2	UB	Х	Х	Х	Х	Х	Х	Х	Х
R24b	HCO+OH<=>CO+H2O	UB	Х	Х	Х	Х	Х	Х	Х	Х
R24p	O2+O+M<=>O3+M	MP	Х	Х	Х	Х	Х	Х	Х	Х
R25a	O+HO2<=>O2+OH	LC	Х	Х	Х	Х	Х	Х	Х	Х
R25b	H+O+O2<=>OH+O2	KPS/MP	Х	Х	Х	Х	IP	Х	Х	Х
R26a	HO2+OH<=>H2O+O2	KPS	С	С	Х	Х	Х	Х	Х	Х
R26b	H2O2+O<=>OH+HO2	UB	Х	Х	Х	Х	Х	Х	Х	Х
R26c	H+OH+O2<=>H2O+O2	KPS/MP	Х	Х	Х	Х	IP	Х	Х	Х
R27	H2O2+OH<=>HO2+H2O	UB	С	С	Х	Х	IP	IP	Х	Х
R30a	HCO+HCO<=>OCHCHO	UB	Х	Х	Х	Х	Х	Х	Х	Х
R30b	HCO+HCO<=>CO+CH2O	UB	Х	Х	Х	Х	Х	Х	Х	Х
R30c	HCO+HCO<=>CO+CO+H2	UB	Х	Х	Х	Х	Х	Х	Х	Х
R30p	CO+O2<=>CO2+O	LC	С	Х	Х	Х	Х	Х	Х	Х
R31a	OHC(O)O+M<=>OHOCO+M	LC	Х	Х	Х	С	Х	Х	Х	Х
R31b	CO2+OH+M<=>OHC(O)O+M	LC	Х	Х	Х	С	Х	Х	Х	Х
R31c	CO2+OH+M<=>OHOCO	LC	Х	Х	Х	С	Х	Х	Х	Х
R31d	CO+HO2<=>OHC(O)O	LC	С	С	С	С	IP	IP	С	IP
R31e	CO+HO2+M<=>OHOCO+M	LC	С	С	С	С	IP	IP	С	IP



R31f	CO+HO2<=>CO2+OH	LC	С	С	С	С	IP	IP	С	IP
R31g	HCO+O2+M<=>OHC(O)O+M	UB	С	С	С	С	IP	IP	С	IP
R31h	HCO+O2+M<=>OHOCO+M	UB	С	С	С	С	IP	IP	С	IP
R31i	HCO+O2<=>CO2+OH	UB	С	С	С	С	IP	IP	С	IP
R31j	HCO+O2<=>CO+HO2	UB	С	С	С	С	IP	IP	С	IP
R32	HCO+HO2<=>CO+H2+O2	UB	Х	Х	Х	Χ	Х	Х	Х	Х
R34	HO2+HO2<=>H2O2+O2	MP	С	С	С	Х	Х	IP	Х	Х

Table 4: Overview of the papers collected for each potential energy surface/reaction and the method use to derive rate constants therein.									
# Electrons	Reaction	Experimental	Theoretical	Detailed Chemical Kinetic Modelling	Total				
R2	H+H+M=H2+M	36	4	1	41				
R9	H+O+M=OH+M	0	0	0	0				
R10	H2O	35	46	0	81				
R11	H2+OH=H2O+H	14	29	0	43				
R15	HCO+M=CO+H+M	18	12	0	30				
R16	H2CO	0	0	0	0				
R16p	O+O+M=O2+M	1	0	0	1				
R17	HO2	82	22	3	107				
R18	H2O2	0	0	0	0				
R19	H3O2	8	6	0	14				
R22	CO+O+M=CO2+M	0	2	0	2				
R23	HCO2	24	29	0	53				
R24	O2+O+M=O3+M	0	3	0	3				
R24p	H2CO2	0	0	0	0				
R25	HO3	10	6	0	16				
R26	H2O3	0	0	0	0				
R27	H2O2+OH=H2O+HO2	5	0	0	5				
R30	H2C2O2	3	1	0	4				
R30p	CO+O2=O+CO2	1	2	0	3				
R31	HCO3	16	4	0	20				
R32	HCO+HO2=CO+H2+O2	0	0	0	0				
R34	HO2+HO2=H2O2+O2	40	4	0	44				
>	Sum	293	170	4	467				



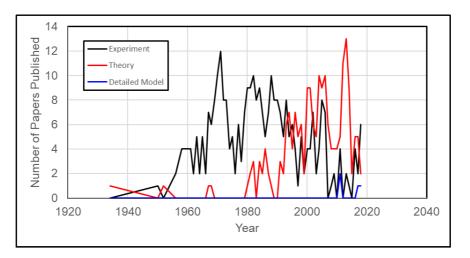


Figure 2: Number of papers published each year with recommended rate constants for reactions in Table 4

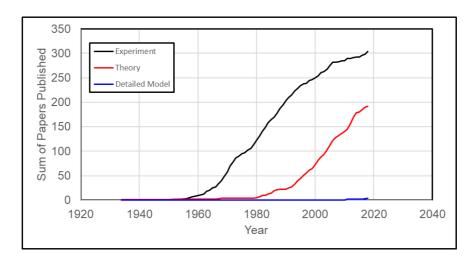


Figure 3: Cumulative number of papers published by a given year which recommend rate constants for reactions in Table 4.



#### Data Fitting for Pressure-Dependent Reactions

For the reaction HCO+M=H+CO+M, approximately 400 unique rate constant measurements have been tabulated based on results from ~17 independent studies, where gas density/pressure, temperature, and bath gas are all variables which influence the reported rate constant, Figure 4. As part of this STSM we have commenced development of a useful procedure to model these data and provide rate constants fits that are both physically meaningful, and useful for combustion modelling.

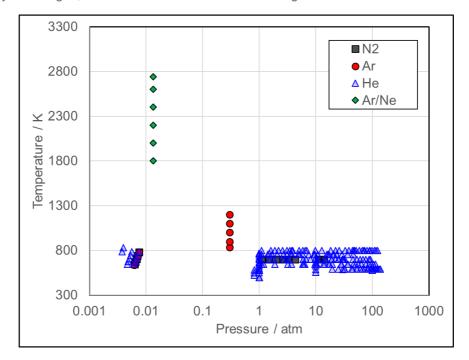


Figure 4: Temperatures and pressures at which the rate constant for HCO+M=H+CO+M has been experimentally measured in various bath gases

Foreach individual experimental measurement, an RRKM/ME input file for use with the MESS solver is constructed based on *ab initio* quantum chemistry results using highly accurate ANLO calculations. The specific temperature, pressure, and bath gas of the experiment is accounted for and each experiment receives an individual treatment. The RRKM/ME master equation results are then compared directly with experimental results.

In order to arrive at optimum fits, some form, the average energy transferred in a collision  $\Delta E_d(T)$  must be described as a function of temperature. A common functional form is  $\Delta E_d(T) = \Delta E_{300}(T/300)^n$  where  $\Delta E_{300}$  is the energy transferred in a collision at 300 K, T, is the temperature, and n is an exponent that describes the temperature dependence of the energy transfer parameter. As part of this STSM, this author develop a computational tool to run large scale RRKM/ME calculations, where  $\Delta E_{300}$  and n are used as variable parameters in the rate constant fitting process. Figure 5-7 below show the result of running approximately 60,000 RRKM/ME calculation in order to find the bath-gas specific values of  $\Delta E_{300}$  and n which give optimal agreement with the available experimental data, as measured by the maximum absolute deviation of the theoretical results from the experimental predictions.

Figure X below shows the results of this work, where heatmaps of the maximum average deviation in the RRKM/ME results are presented as a function of  $\Delta E_{300}$  and the fitting exponent n. What is clear is that there are potentially multiple minima as part of this fitting procedure, and there may not be unique values of  $\Delta E_{300}$  and the fitting exponent n which give best agreement with the data.



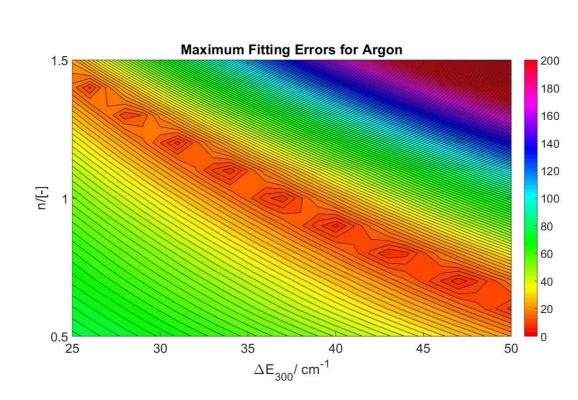


Figure 5: Fitting errors (Maximum Absolute Deviation) of the RRKM/ME calculations, from the experimental data for Ar bath gas.

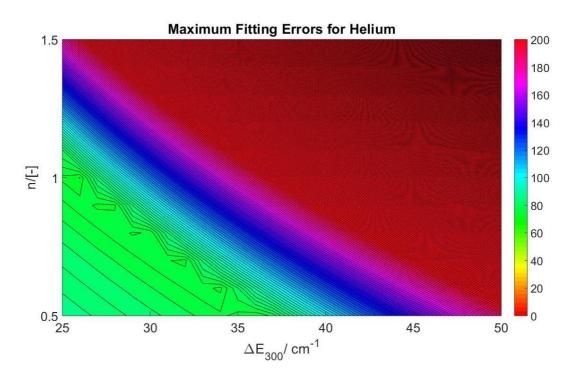


Figure 6: Fitting errors (Maximum Absolute Deviation) of the RRKM/ME calculations, from the experimental data for He bath gas.



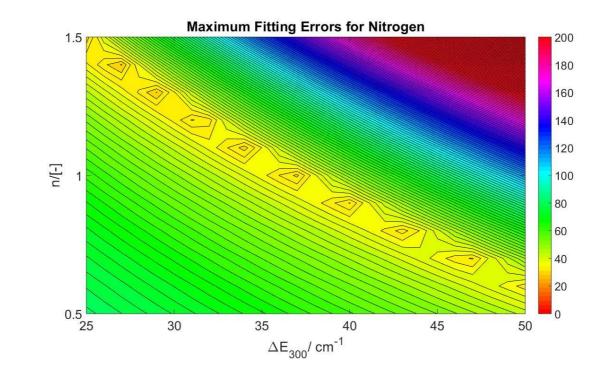


Figure 7: Fitting errors (Maximum Absolute Deviation) of the RRKM/ME calculations, from the experimental data for  $N_2$  bath gas.

The results presented above are also bath-gas specific, with different values of  $\Delta E_{300}$  and the fitting exponent n found to best reproduce the data in different bath gases. For a given bath gas, the lack of a unique values of  $\Delta E_{300}$  and the fitting exponent n complicate the procedure of producing rate constants for use in kinetic models, as these parameters will become increasingly sensitive under high temperature and low-pressure conditions which are beyond the temperature pressure range of the current kinetic data, but which are typical of combustion conditions (e.g. shock tubes, flames, engines). Future work will aim to refine this fitting procedure to incorporate other aspects of the potential energy surface, including the reaction barrier, and the imaginary frequency of the reaction path.

#### **FUTURE COLLABORATIONS (if applicable)**

The same approach will be applied to all of the remaining reactions listed below:

R2: H + H + M => H2 + M

R9: H + O + M => OH + M

R10a: H + OH (+M) => H2O (+M)

R10b: H2 + O => H + OH

R11: H2 + OH => H2O + H

R15: HCO (+M) => CO + H (+M)

R16: HCO + H => CO + H2

R16p: O + O + M => O2 + M

R17a: H + O2 (+M) => HO2 (+M)

R17b: H + O2 => O + OH

R-17b: O + OH => H + O2R18a: OH + OH (+M) => H2O2

R18b: OH + OH => O + H2O



R18c: H + H02 => H2 + 02R18d: H + H02 => OH + OHR18e: H + H + O2 => H2 + O2R18f: H + H + O2 => OH + OHR22: CO + O (+M) => CO2 (+M)R23a: CO2 + H => HOCO R23b: CO + OH => HOCOR23c: CO + OH => CO2 + H R23d: HCO + O => CO2 + HR23e: HCO + O => CO + OH R24: O2 + O(+M) => O3(+M)R24pa: HCO + OH => CO2 + H2R24pb: HCO + OH => CO + H2OR25a: O + HO2 => O2 + OHR25b: H + O + O2 => OH + O2R26a: OH + HO2 => H2O + O2R26b: H202 + 0 => H20 + 02R26c: H + OH + O2 => H2O + O2R27: H202 + OH => H20 + H02R30a: HCO + HCO => OCHCHO R30b: HCO + HCO => CO + H2CO R30c: HCO + HCO => CO + CO + H2 R30p: CO + O2 => CO2 + OR31a: OHC(0)0 (+M) => OHOCO (+M) R31b: CO2 + OH (+M) => OHC(O)O (+M)R31c: CO2 + OH (+M) => OHOCO (+M)R31d: CO + HO2 => OHC(O)O (+M)R31e: CO + HO2 (+M) => OHOCO (+M)R31f: CO + HO2 => CO2 + OH R31g: HCO + O2 (+M) => OHC(O)O (+M)R31h: HCO + O2 (+M) => OHOCO (+M)R31i: HCO + O2 => CO2 + OH R32: HCO + HO2 => CO + O2 + H2R34: H02 + H02 => H202 + 02

The working group has decided to meet on bi-weekly telecons, in order to continue progress on the review of the above listed reactions.

A publication to be submitted to Progress in Energy and Combustion Science or, alternatively, to the Journal of Physical and Chemical Reference Data is expected by March 2019.

The progresses of this activity will be presented at the final SMARTCATs meeting and 1<sup>st</sup> International Conference on Smart Energy Carrier to be held in Naples on the 21<sup>st</sup>-23<sup>rd</sup> of January 2019.

As part of this author's future work, a scientific exchange to Dr. Stephen Klippenstein at Argonne National Laboratory is planned in order to continue developing the methods described herein. That trip is due to take place in Spring 2019.